

# Improved Analytical Approach for Fuel Demand Re-Evaluation in Liquid and Gaseous Waste Thermal Processing Units

Dr. Zdeněk Jegla, Vít Freisleben, Martin Krňávek



November 2021

# RESEARCH GROUP



**Dr. Zdeněk Jegla**

Associate professor  
Institute of Process Engineering  
BUT, Czech Republic



**Vít Freisleben**

Feasibility study and research  
EVECO Brno, Czech Republic



**Martin Krňávek**

Combustion technology and  
heat transfer specialist  
EVECO Brno, Czech Republic

# PRESENTATION CONTENT

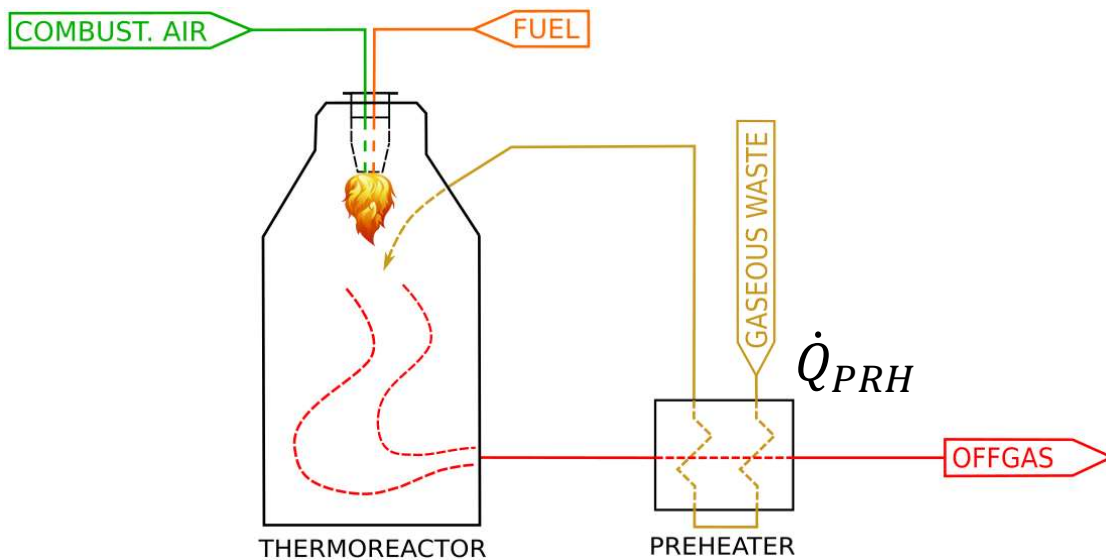
---

- **Waste Thermal Processing Units (WTPU) for processing:**
  - **Gaseous waste**
  - **Liquid waste**
- **Existing calculation method for supplemental fuel saving evaluation.**
- **Comparative non-linear (SRK) model.**
- **Improvement of existing calculation procedure**
- **Case studies**

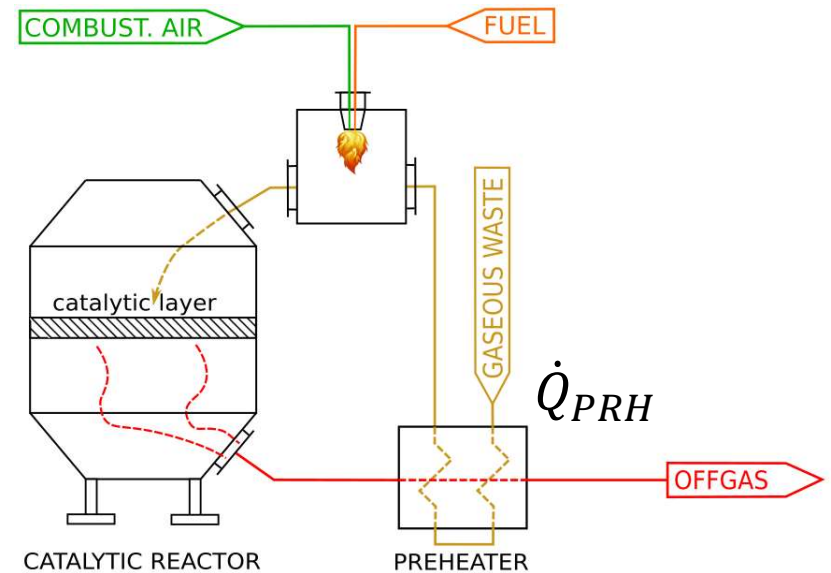
# WASTE THERMAL PROCESSING UNITS

## Gaseous waste processing

### Thermal decomposition

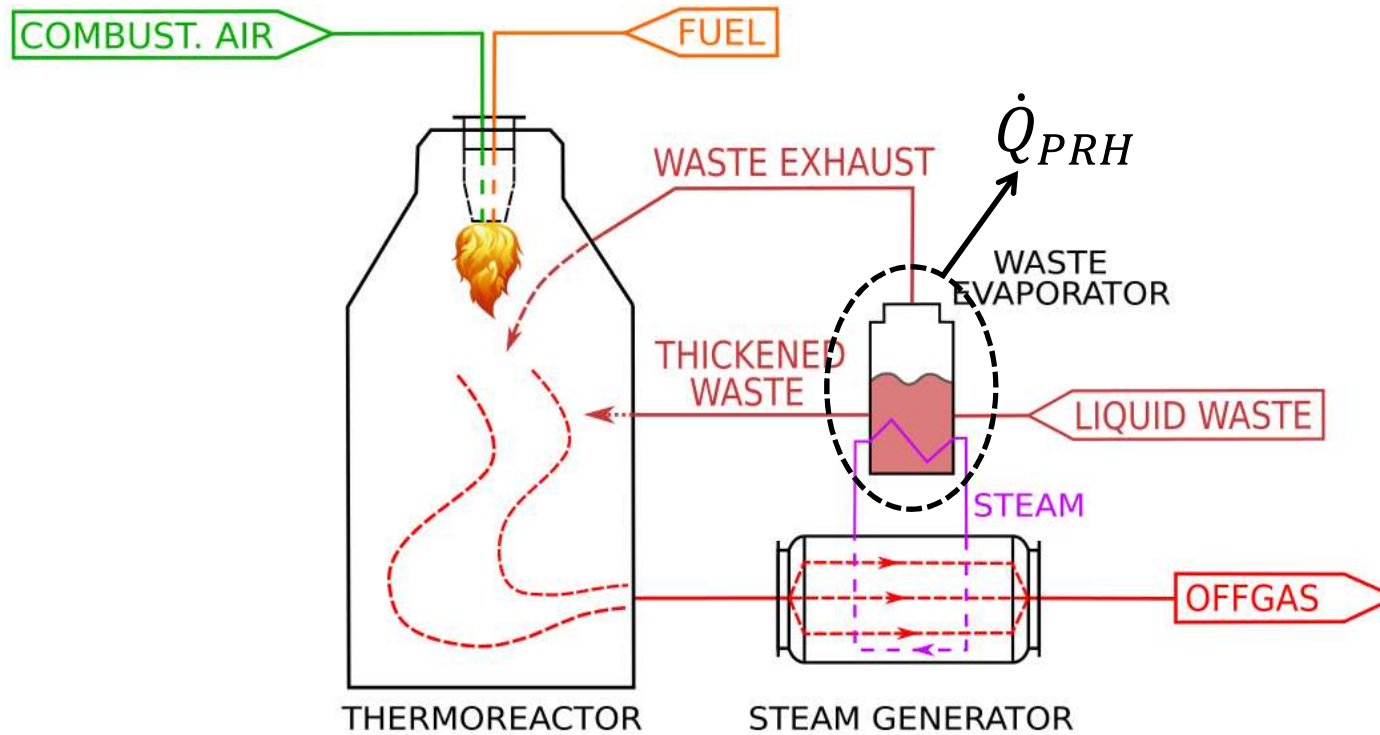


### Catalytic decomposition



# WASTE THERMAL PROCESSING UNITS

## Liquid waste processing



# SUPPLEMENTAL FUEL SAVING EVALUATION

## Previous research

V. Freisleben and Z. Jegla, 'Innovative Method for Fuel Saving Calculation Related to Energy Retrofit of Thermal Waste Processing Units', in *Proceedings of the 26th Conference Eng. Mech.*, Svatka, 2020, vol. 10, pp. 142–145.

$$\Delta f_s = \dot{Q}_{PRH} / FHV_{CC}$$
$$FHV_{CC} = LHV \cdot n_c \cdot \frac{T_{adiab} - T_{CC}}{T_{adiab} - T_{init}}$$

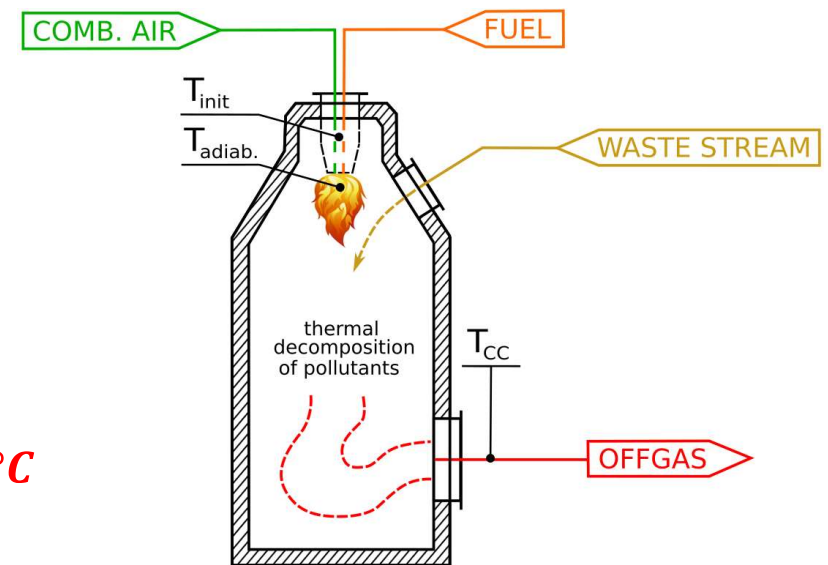
$$n_c = (1.07; 1.09)$$

## Gaseous waste processing units retrofit

V. Freisleben and Z. Jegla, „Conceptual Design Method for Energy Retrofit of Waste Gas-to-Energy Units", *J. sustain. dev. energy water environ. syst.*, vol. 10, 2021, (in press).

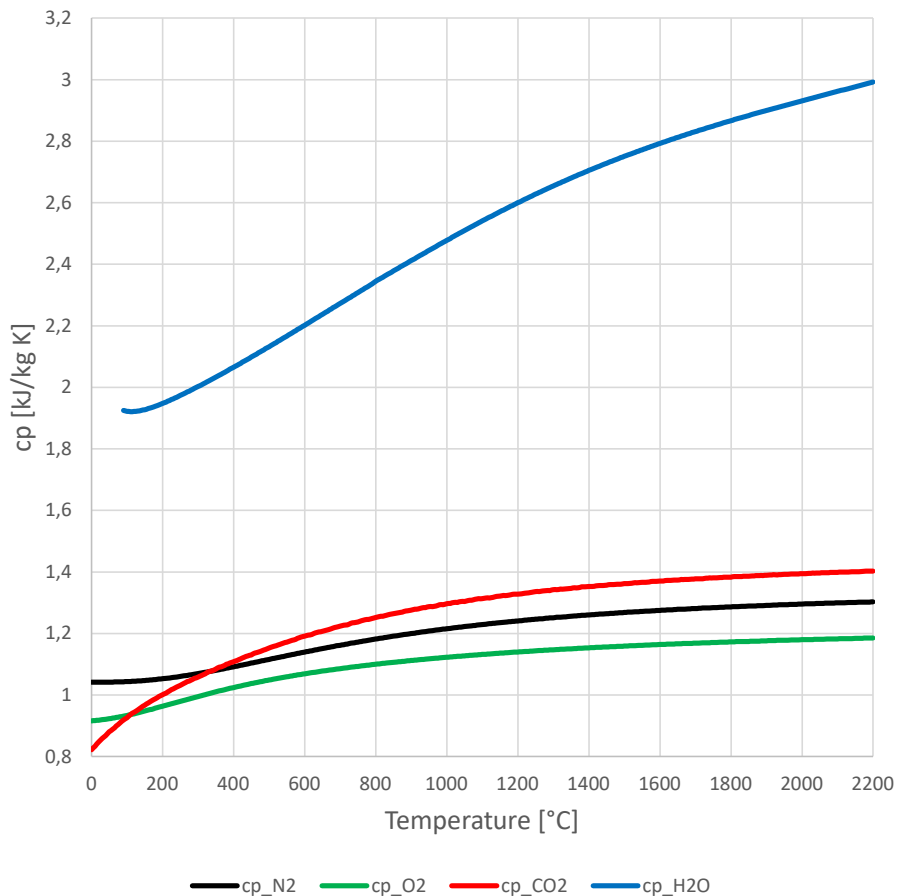
Reliable relationship only for  $T_{CC} \approx 800 \text{ }^\circ\text{C}$  and  $T_{init} \approx 20 \text{ }^\circ\text{C}$

Goal: finding relationship for reliable  $\Delta f_s$  calculation in wider temperature range, i.e. for any WTPU



# FLUE GAS PROPERTIES - SRK MODEL

Spec. heat capacity functions for flue gas components  
(SRK model)



Soave–Redlich–Kwong (SRK) model:

$$c_p = a \cdot T^4 + b \cdot T^3 + c \cdot T^2 + d \cdot T + e$$

**H<sub>2</sub>O:**

$$\begin{aligned} a &= 9.44 \cdot 10^{-14} \\ b &= -5.05 \cdot 10^{-10} \\ c &= 7.79 \cdot 10^{-7} \\ d &= 2.29 \cdot 10^{-4} \\ e &= 1.8791 \end{aligned}$$

**CO<sub>2</sub>:**

$$\begin{aligned} a &= -3.71 \cdot 10^{-1} \\ b &= 2.44 \cdot 10^{-10} \\ c &= -6.52 \cdot 10^{-7} \\ d &= 9.01 \cdot 10^{-4} \\ e &= 0.8389 \end{aligned}$$

**N<sub>2</sub>:**

$$\begin{aligned} a &= 4.82 \cdot 10^{-14} \\ b &= -2.27 \cdot 10^{-10} \\ c &= 2.91 \cdot 10^{-7} \\ d &= 0.69 \cdot 10^{-4} \\ e &= 1.0334 \end{aligned}$$

**O<sub>2</sub>:**

$$\begin{aligned} a &= -6.75 \cdot 10^{-16} \\ b &= 0.37 \cdot 10^{-10} \\ c &= -1.88 \cdot 10^{-7} \\ d &= 3.74 \cdot 10^{-4} \\ e &= 0.9014 \end{aligned}$$

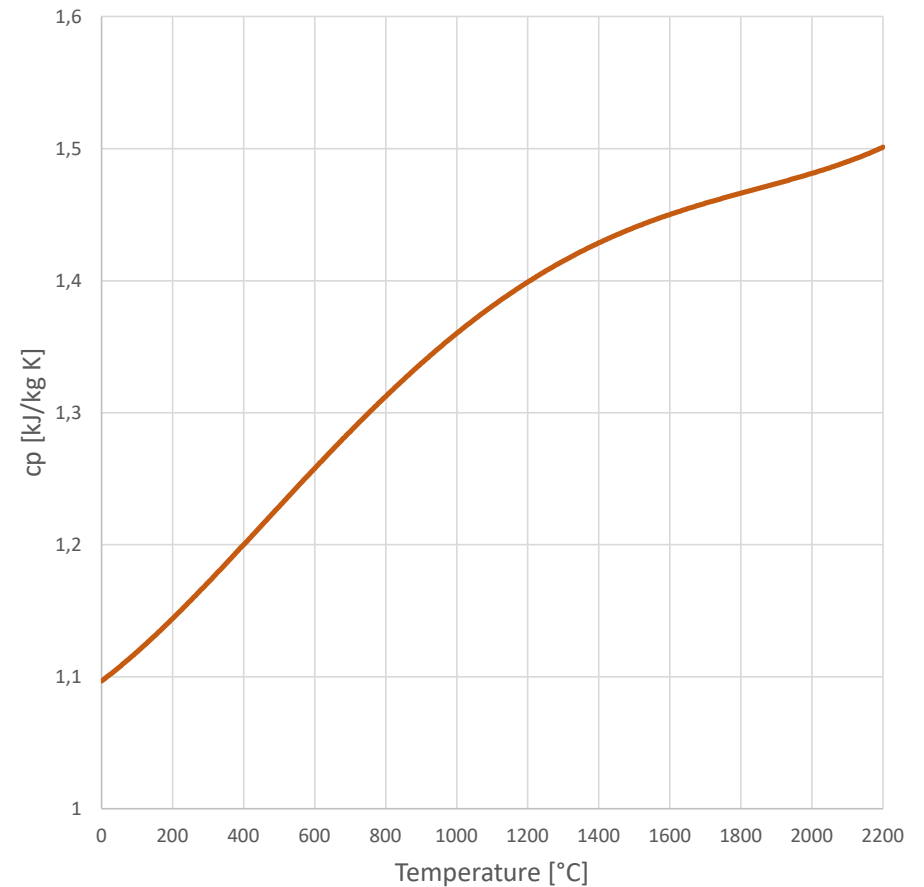
# FLUE GAS PROPERTIES - SRK MODEL

$$c_{pFlueGas} = \sum_{comp.} w_i \cdot c_{p i}$$
$$= w_{H_2O} \cdot c_{p H_2O} + w_{CO_2} \cdot c_{p CO_2} + w_{N_2} \cdot c_{p N_2} + w_{O_2} \cdot c_{p O_2}$$

$w_i$  - weight fraction of component in flue gas

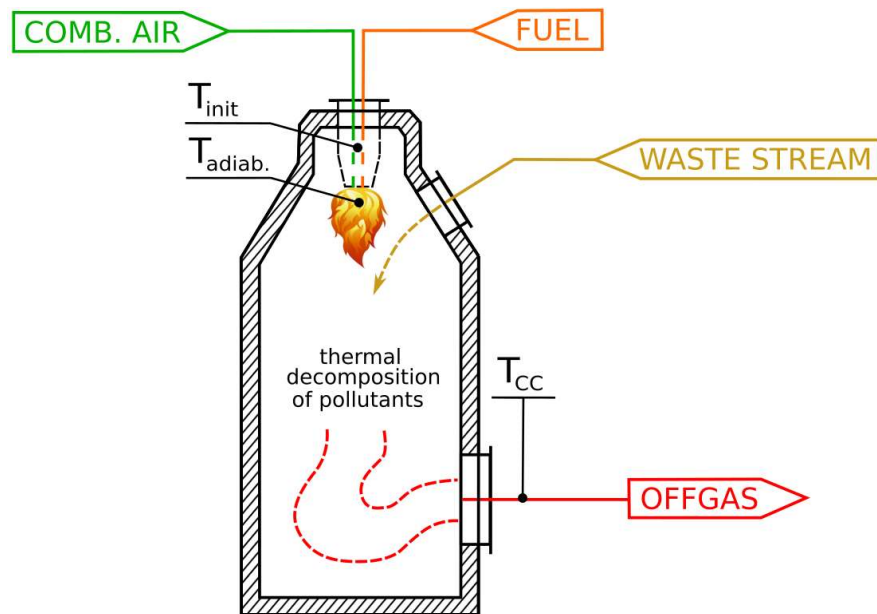
$c_{p i}$  - spec. heat capacity of component in flue gas

Spec. heat capacity function of flue gas from CH<sub>4</sub> combustion with 5% air excess (SRK model)

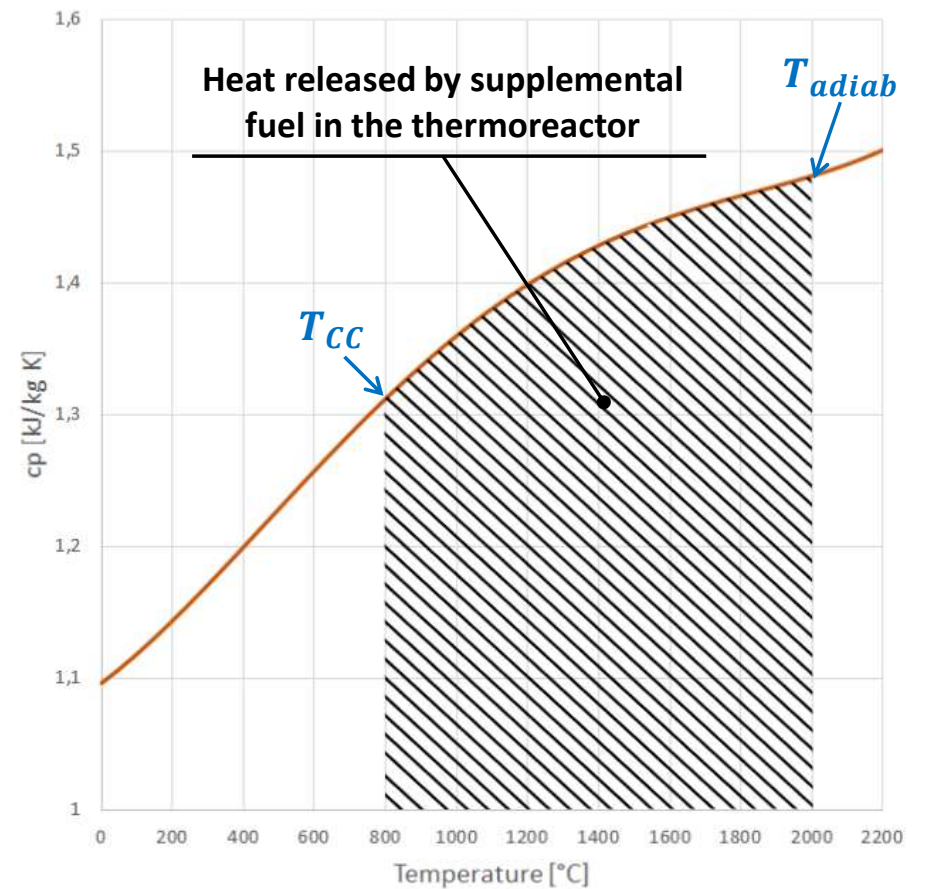




# FUEL'S HEAT CONTENT IN THERMOREACTOR



Spec. heat capacity function of flue gas from CH<sub>4</sub> combustion with 5% air excess (SRK model)



# LINEAR APPROXIMATION OF SRK MODEL

## Initial problem

$$n_{c\_nonlin} = \frac{T_{adiab} - T_{init}}{T_{adiab} - T_{CC}} \cdot \frac{\int_{T_{CC}}^{T_{adiab}} c_{pFlueGas} dT}{\int_{T_{init}}^{T_{adiab}} c_{pFlueGas} dT}$$

$$n_{c\_lin} = K_1 \cdot T_{CC} + K_2 \cdot T_{init} + K_3 \cdot T_{adiab} + K_4$$

(500; 1100)°C      (0; 400)°C      (1800; 2200)°C

*objective* →  $\min\{|n_{c\_nonlin} - n_{c\_lin}|\}$

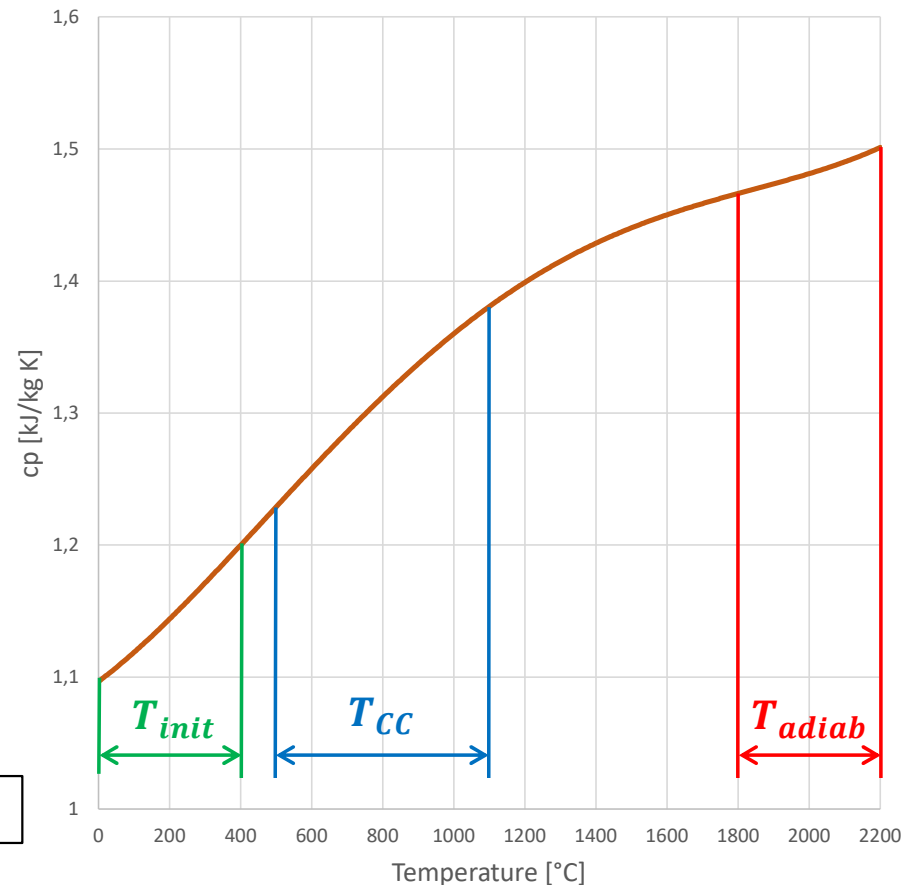
## Process

Optimization of the values  $K_1, K_2, K_3$  and  $K_4$  to find the best linear approximation of SRK model

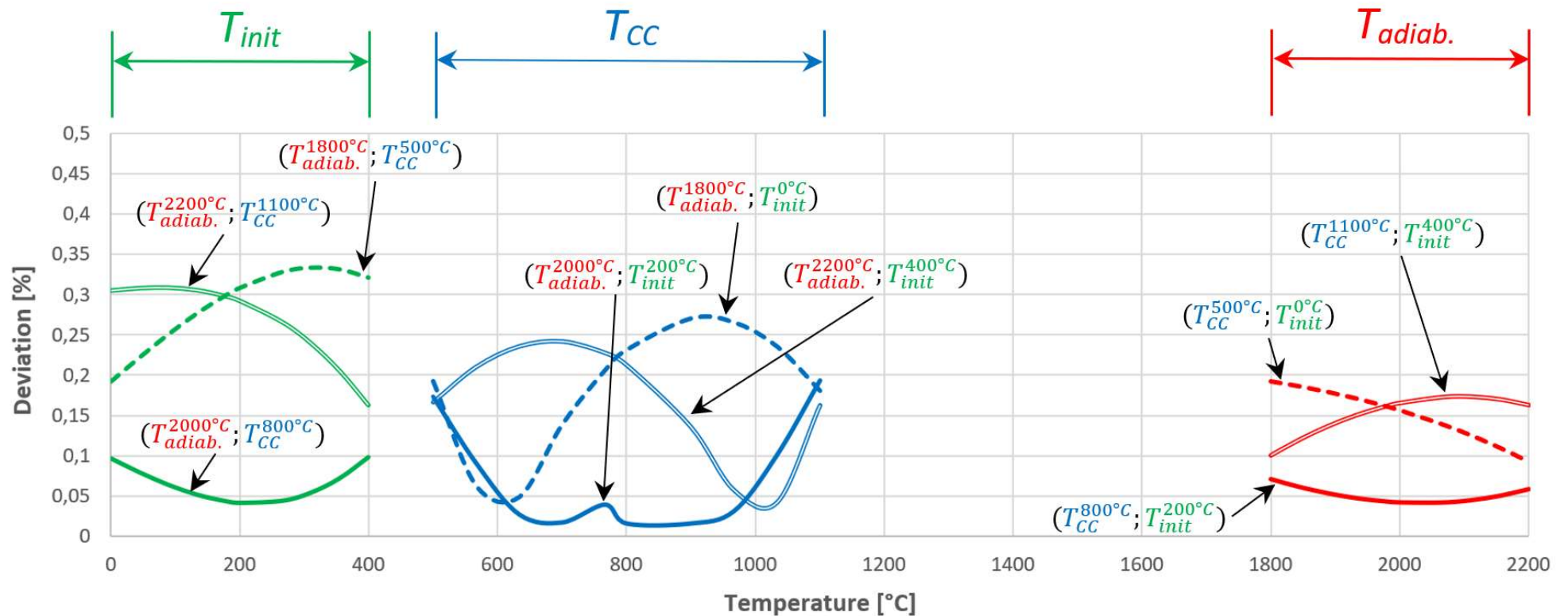
## Result

$$n_{c\_lin} = (6,462 \cdot T_{CC} - 8,969 \cdot T_{init} - 1,467 \cdot T_{adiab}) \cdot 10^{-5} + 1,0416$$

Spec. heat capacity function of flue gas from CH<sub>4</sub> combustion with 5% air excess (SRK model)



# LINEAR/NON-LINEAR MODEL COMPARISON



# CASE STUDIES

The developed calculation procedure is applied on both, the gaseous waste processing units and liquid waste processing units. In all studies, the supplemental fuel is natural gas combusted in the burner with 5% excess of combustion air. The results are compared to the non-linear simulation based on the SRK model.

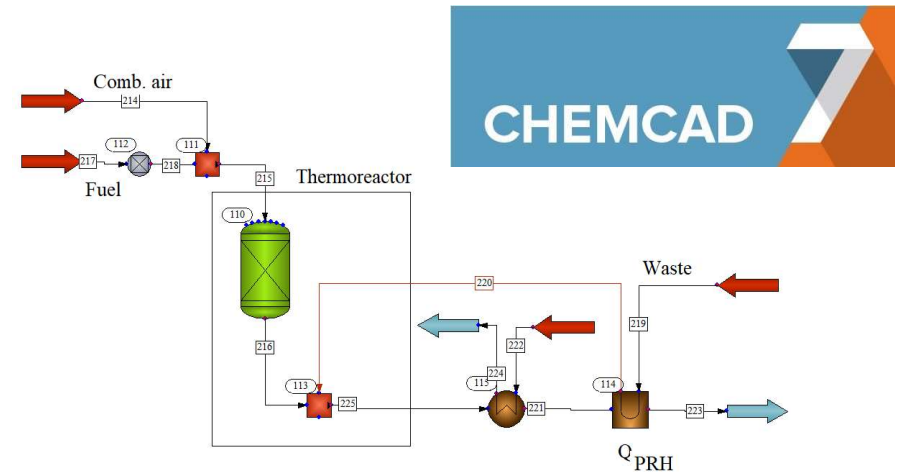
## Linear model

$$\Delta f_s = \dot{Q}_{PRH} / FHV_{CC}$$

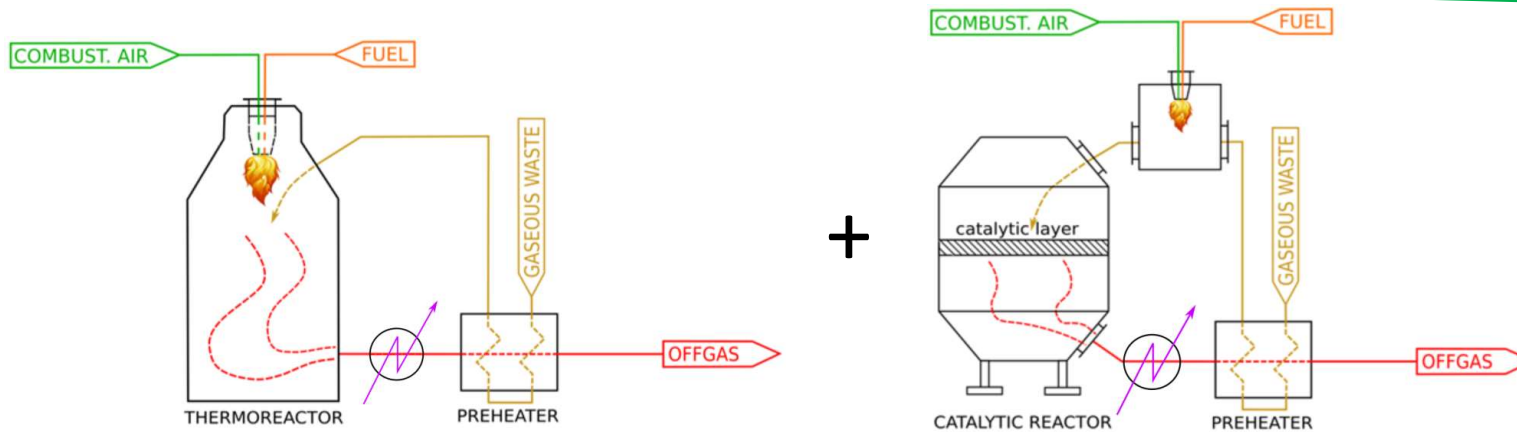
$$FHV_{CC} = LHV \cdot n_c \cdot \frac{T_{adiab} - T_{CC}}{T_{adiab} - T_{init}}$$

$$n_c = (6,462 \cdot T_{CC} - 8,969 \cdot T_{init} - 1,467 \cdot T_{adiab}) \cdot 10^{-5} + 1,0416$$

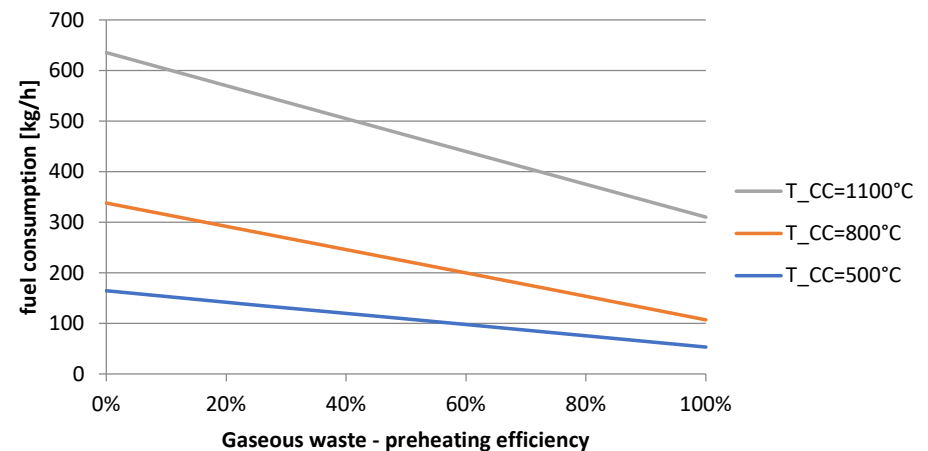
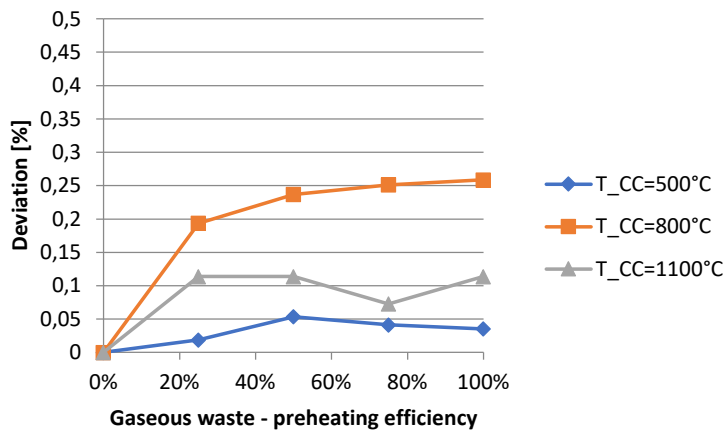
## Non-linear model



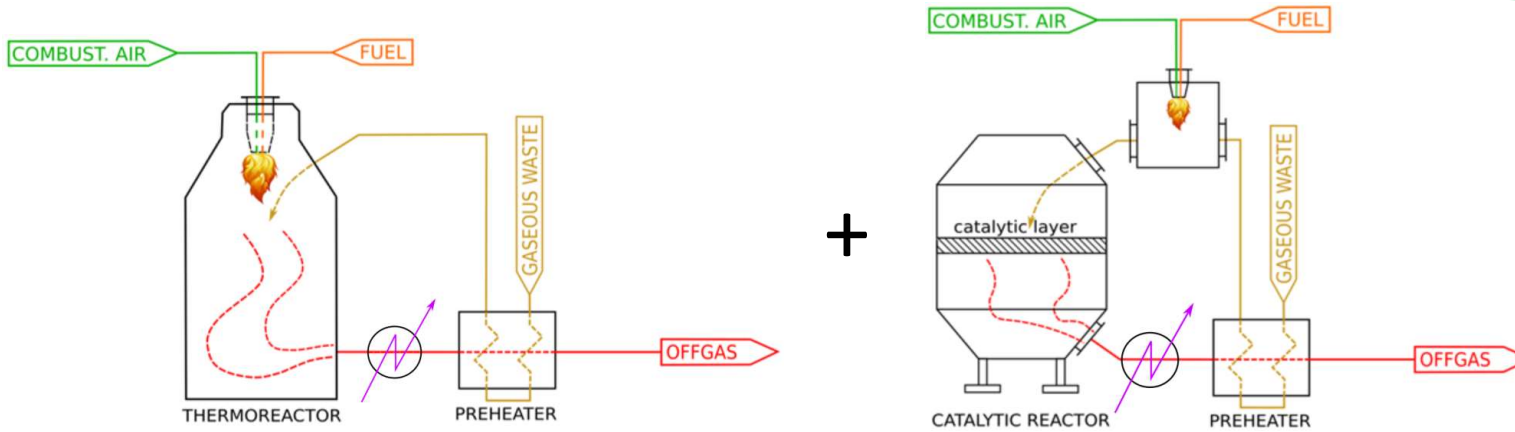
# CASE STUDY 1: WTPU – GASEOUS WASTE



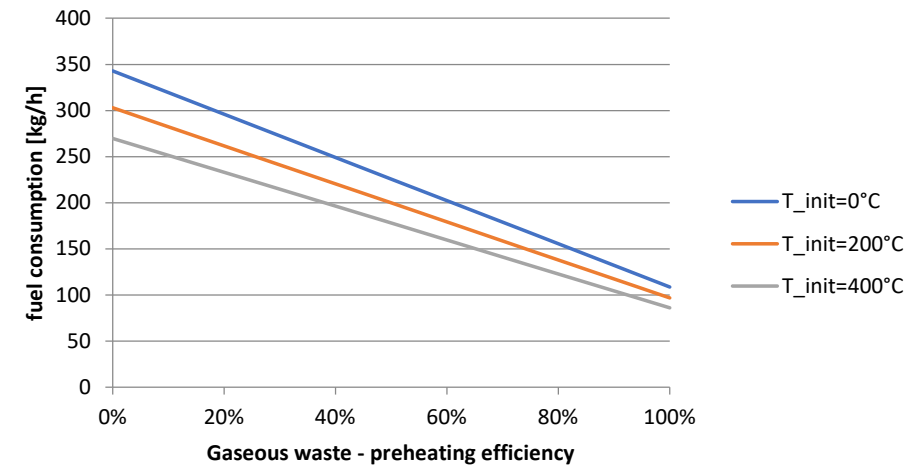
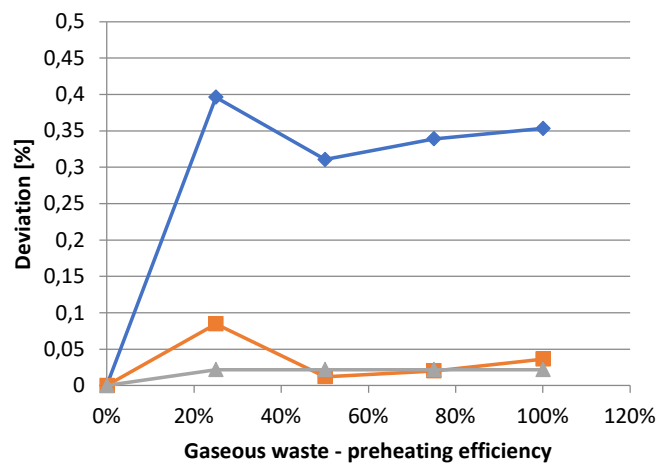
Variables:  $T_{CC}$  and  $Q_{PRH}$  (in terms of HE's efficiency)



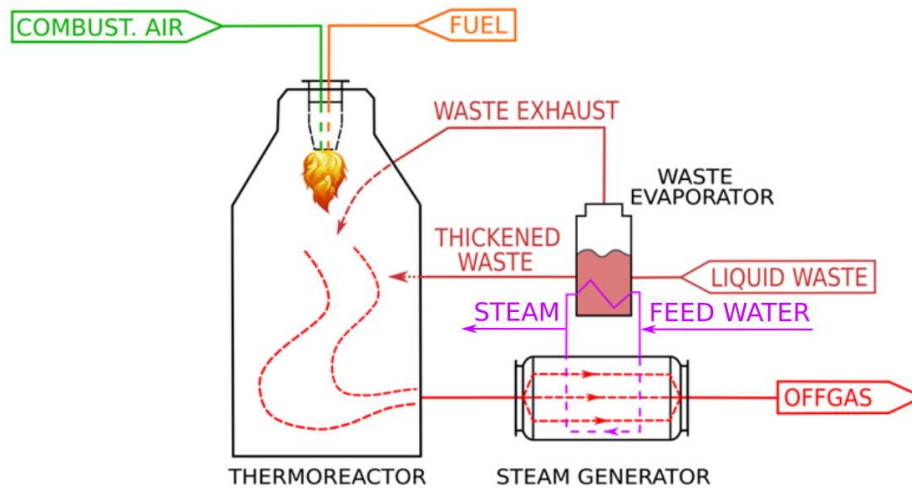
# CASE STUDY 1: WTPU – GASEOUS WASTE



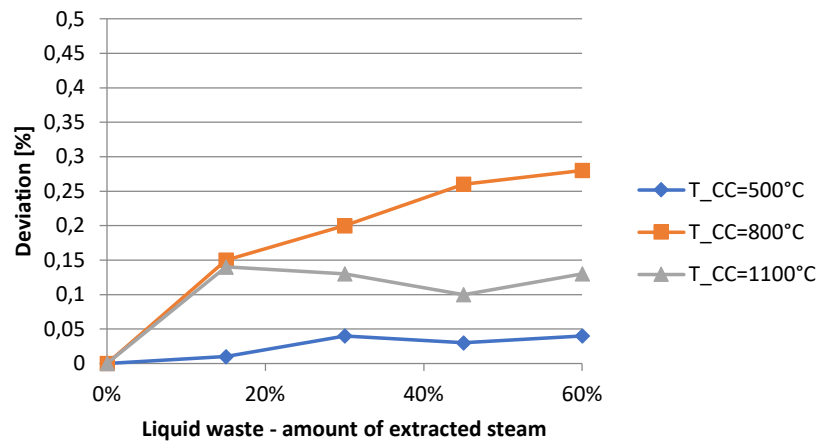
Variables:  $T_{init}$  and  $Q_{PRH}$  (in terms of HE's efficiency)



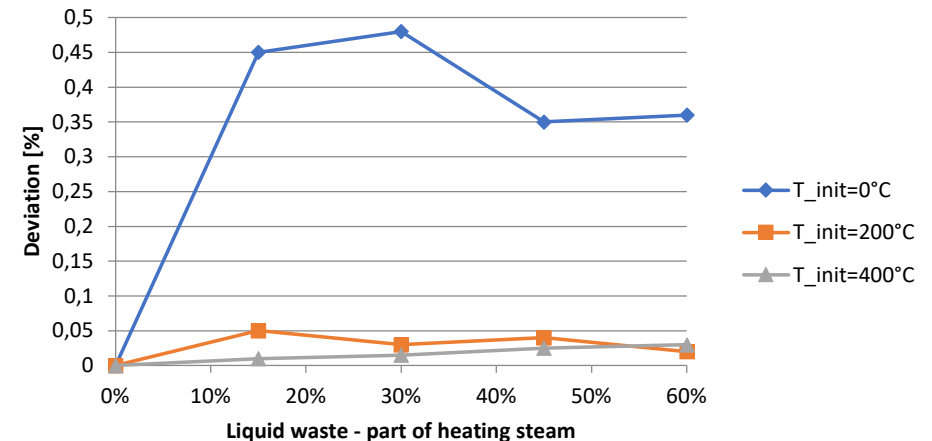
# CASE STUDY 2: WTPU – LIQUID WASTE



Variables:  $T_{CC}$  and  $Q_{PRH}$  (amount of heating steam)



Variables:  $T_{init}$  and  $Q_{PRH}$



# CONCLUSION AND FUTURE WORK

---

- **Within this research, a reliable and simple calculation procedure was proposed in order to describe the relationship between the waste thermal pre-treatment, and consequent supplemental fuel saving. The procedure is applicable to any WTPU with similar technology arrangement, as presented here. The results' accuracy is not dependent on the heating intensity, so the developed procedure can be applied to the WTPU of any size or preheating efficiency.**
- **In the future work, the developed procedure will be implemented to the, co-called, CDM (Conceptual Design Method) in order to extend the CDM's applicability to the retrofit of WTPUs processing liquid wastes, and catalytic WTPUs processing gaseous wastes.**



# SUPPORTING PROJECTS

- **CZ.02.1.01/0.0/0.0/16\_026/0008413** – „Strategic Partnership for Environmental Technologies and Energy Production “



EUROPEAN UNION  
European Structural and Investment Funds  
Operational Programme Research,  
Development and Education



- **LTACH19033** – „Transmission Enhancement and Energy Optimised Integration of Heat Exchangers in Petrochemical Industry Waste Heat Utilisation “



INTER-EXCELLENCE



# THANK YOU!

Dr. Zdeněk Jegla, Vít Freisleben, Martin Krňávek



November 2021